

# Catalytic Heat Exchanger for SOFC Balance-of-Plant Cost Reduction

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## Project Objective

Demonstrate conceptual feasibility of a highly effective catalytic cathode air preheater for a 60kW SOFC power plant to increase plant performance and to reduce the balance of plant cost.

## Team Partners

FuelCell Energy, Inc.  
Danbury, CT



FuelCell Energy

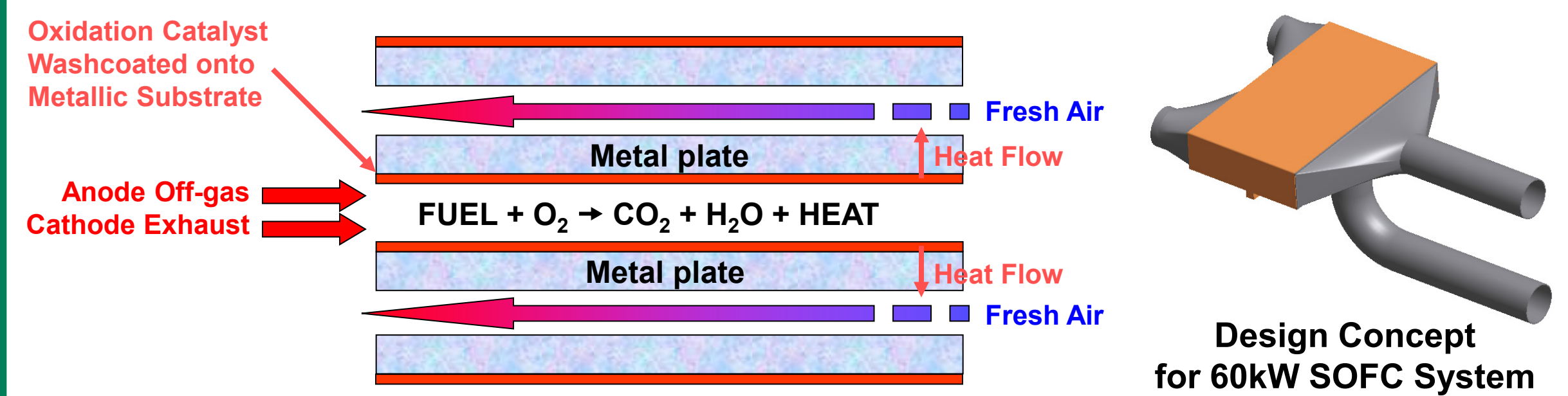
BASF Catalysts  
Iselin, New Jersey



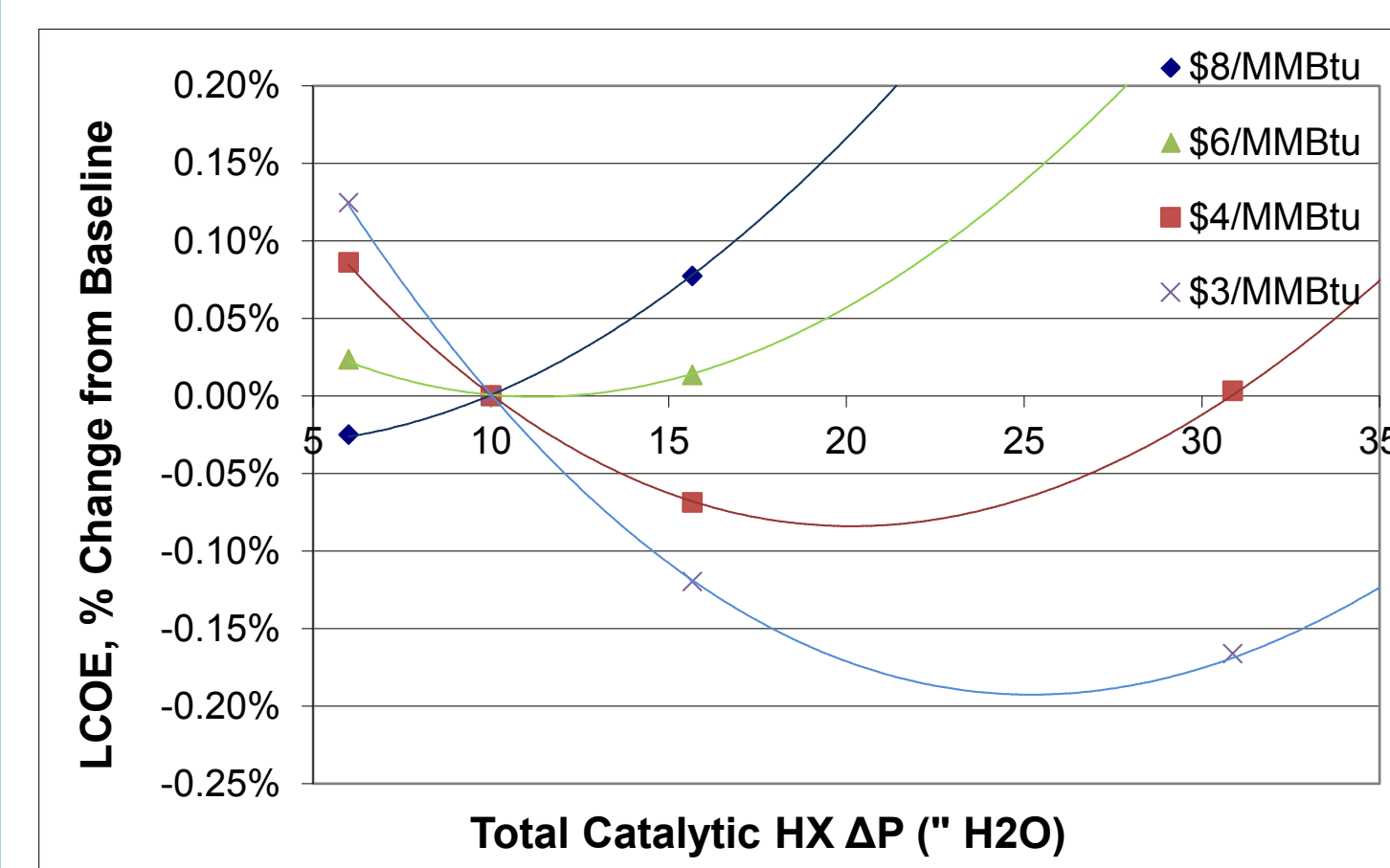
Modine  
Manufacturing Co.  
Racine, WI



## Conceptual Catalytic Heat Exchanger Design for 60kW SOFC Power Plant



## Sensitivity Study: Levelized Cost of Electricity (LCOE) vs. Catalytic HX Pressure Drop Specification



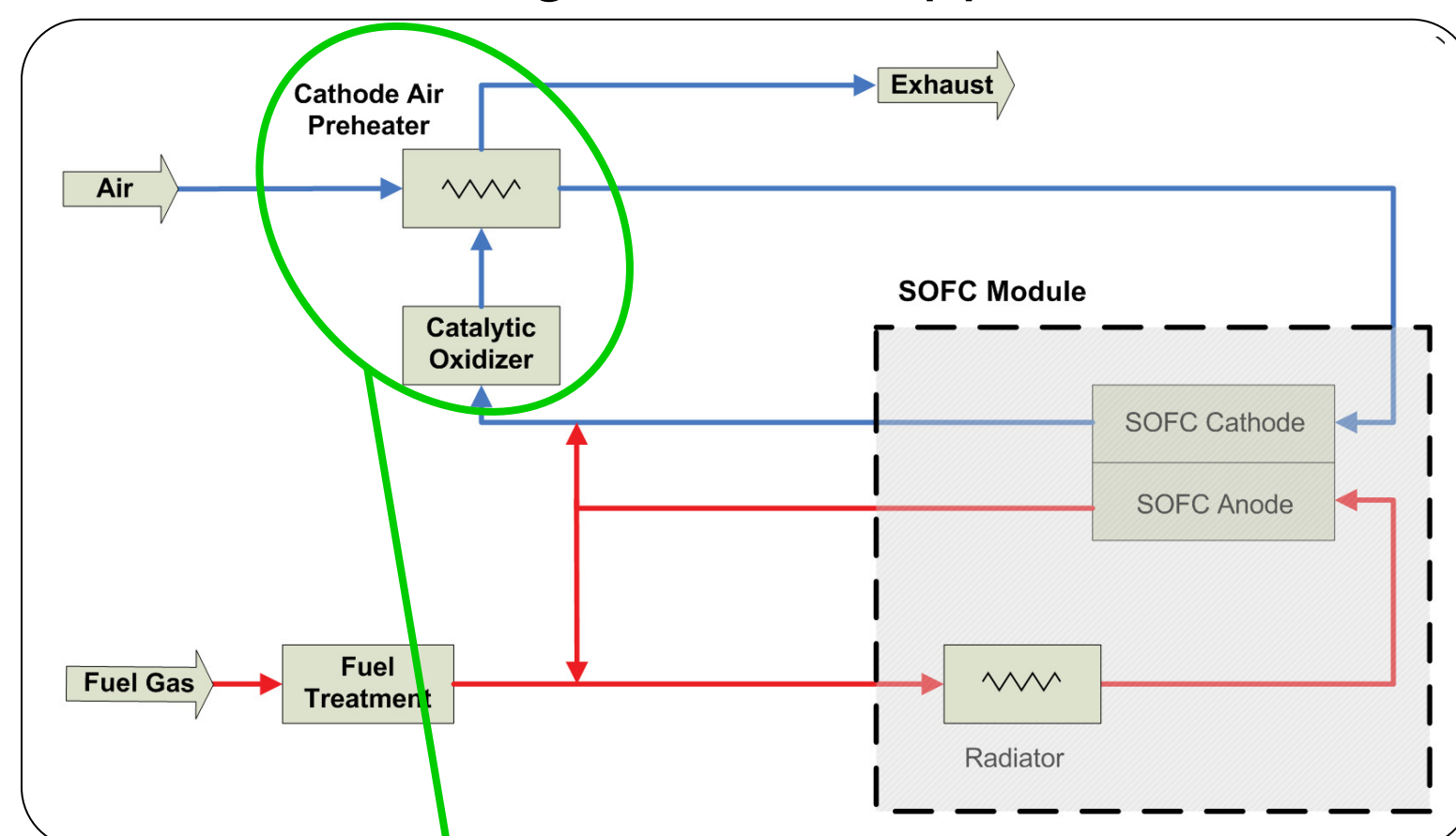
Natural Gas Price (\$/MMBtu)	HX dP for minimal LCOE ("H <sub>2</sub> O)	Net Plant Efficiency @ Min. LCOE dp Allowance (LHV NG)
\$8.00	<6	<59.5%
\$6.00	10.5	61.3%
\$4.00	20	61.0%
\$3.00	25	60.9%

- As fuel prices decrease from \$8/MMBtu to \$3/MMBtu, optimal dP specification increases from <6 to 25"H<sub>2</sub>O

## Project Background

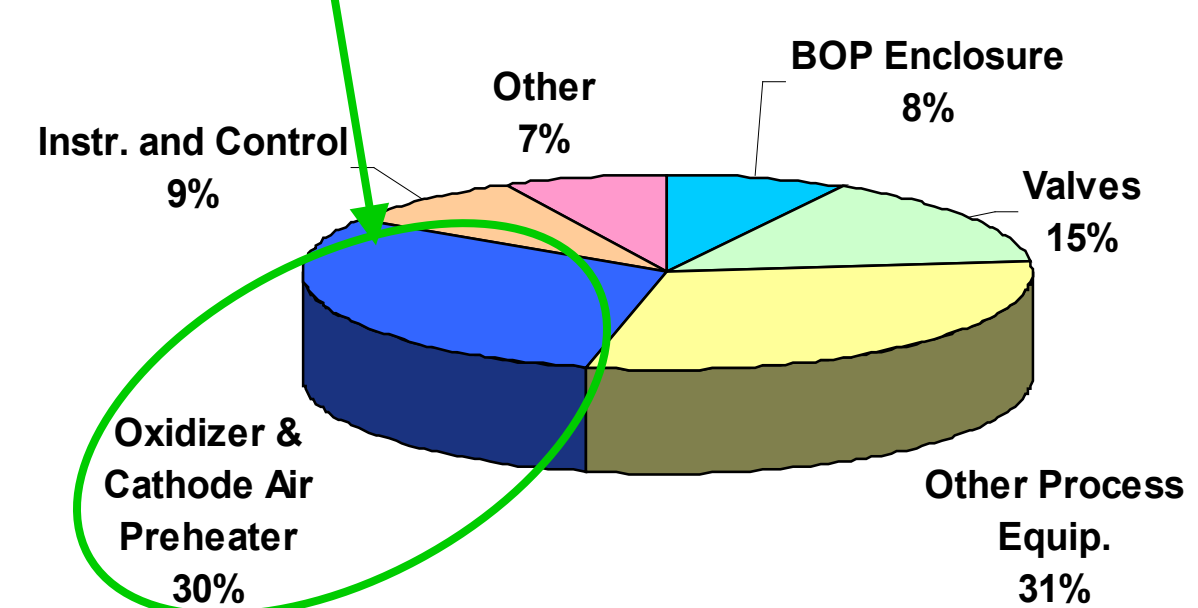
- In addition to SOFC cell/stack performance, cost, and durability improvements – innovative technologies for reducing balance-of-plant (BOP) component costs are required for successful commercial deployment of SOFCs in distributed generation applications.

### Typical SOFC-based System

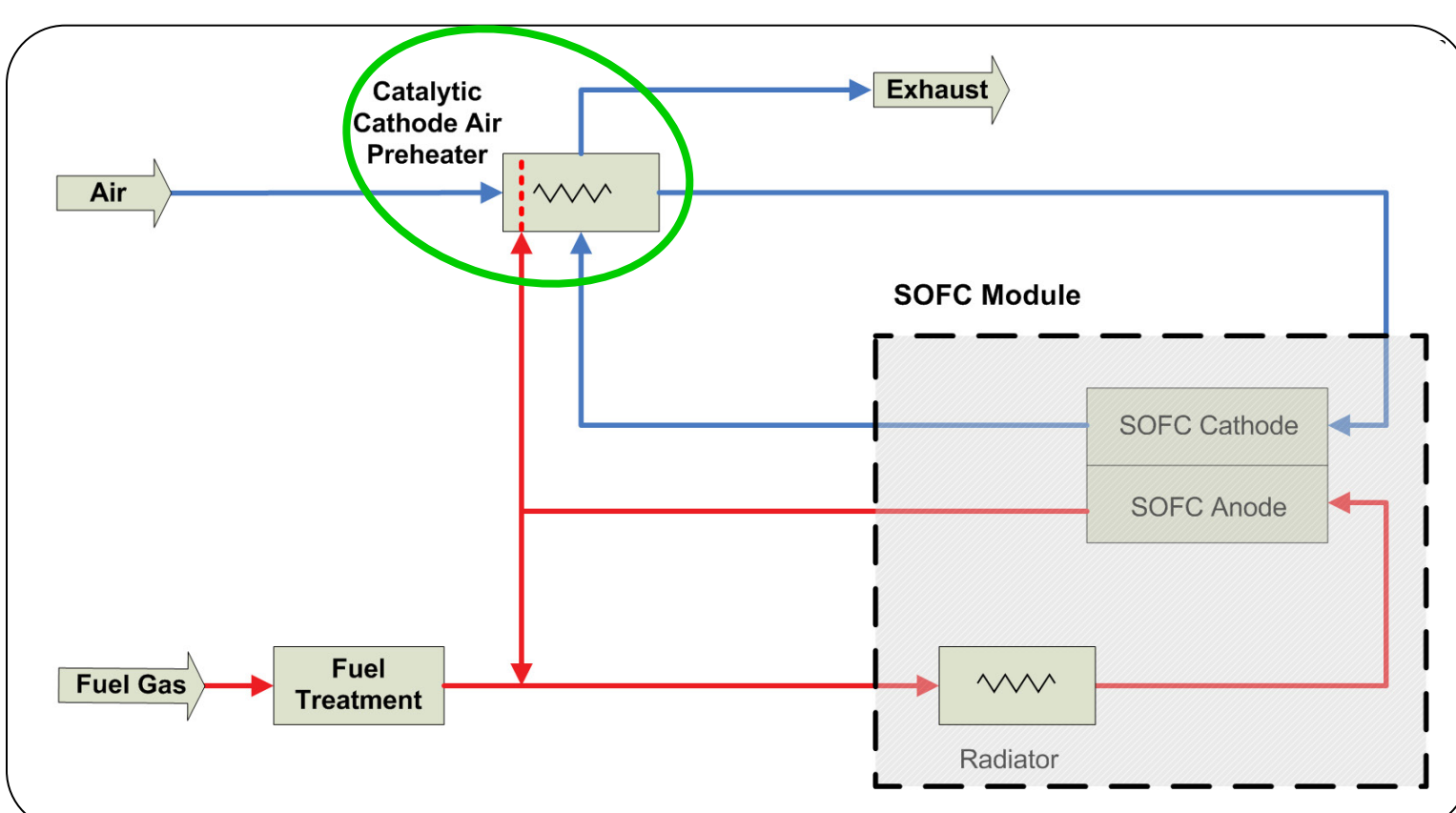


### BOP Capital Equipment Cost Breakdown:

Oxidizer and Air Preheater represent the largest opportunity for BOP cost reductions

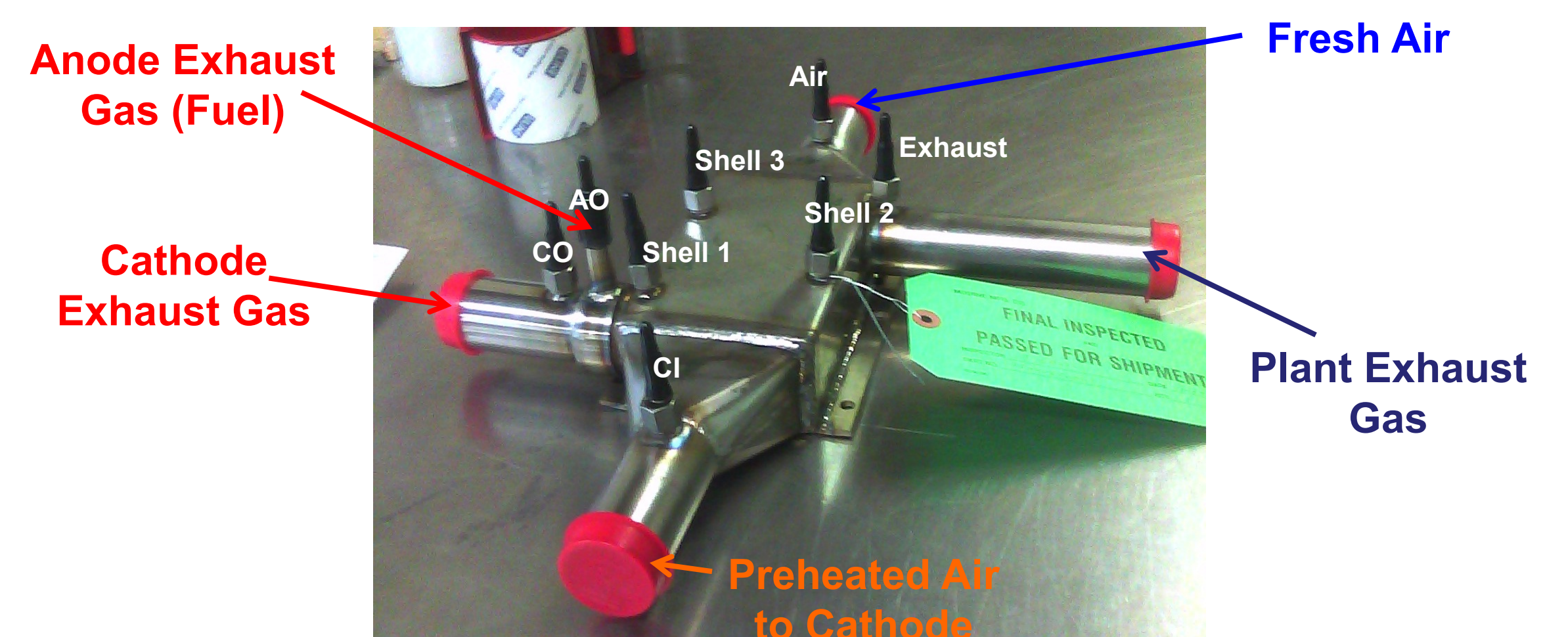


### Simplified System Concept with Multi-Functional Catalytic Heat Exchanger



60-80% cost reduction estimated (in high volume production), compared to conventional separate oxidizer / heat exchanger

## Lab-Scale (3kW<sub>e</sub>) Catalytic Heat Exchanger Design and Fabrication



- Provisions for pressure measurement at each inlet and outlet
- Provisions for thermocouples at each inlet and outlet, in addition to 3 thermocouples to map shell-side temperatures

## Lab-Scale Catalytic Heat Exchanger Testing Results

- Maximum combustion temperature was well-controlled
  - No temperature run-away observed
  - Maximum combustion temperature is effectively moderated even up to 2X the design fuel flow rate
- Hot-in to cold-out approach temperatures:
  - 94 °C without fuel flow (non-catalytic mode)
  - 19.4 °C with fuel flow (catalytic mode)
- Heat duty
  - As tested = 2.85 kW (test facility maximum temperature limited)
- Total pressure drop at Normal Operating Conditions = 7.8 "H<sub>2</sub>O (below 10 "H<sub>2</sub>O target)

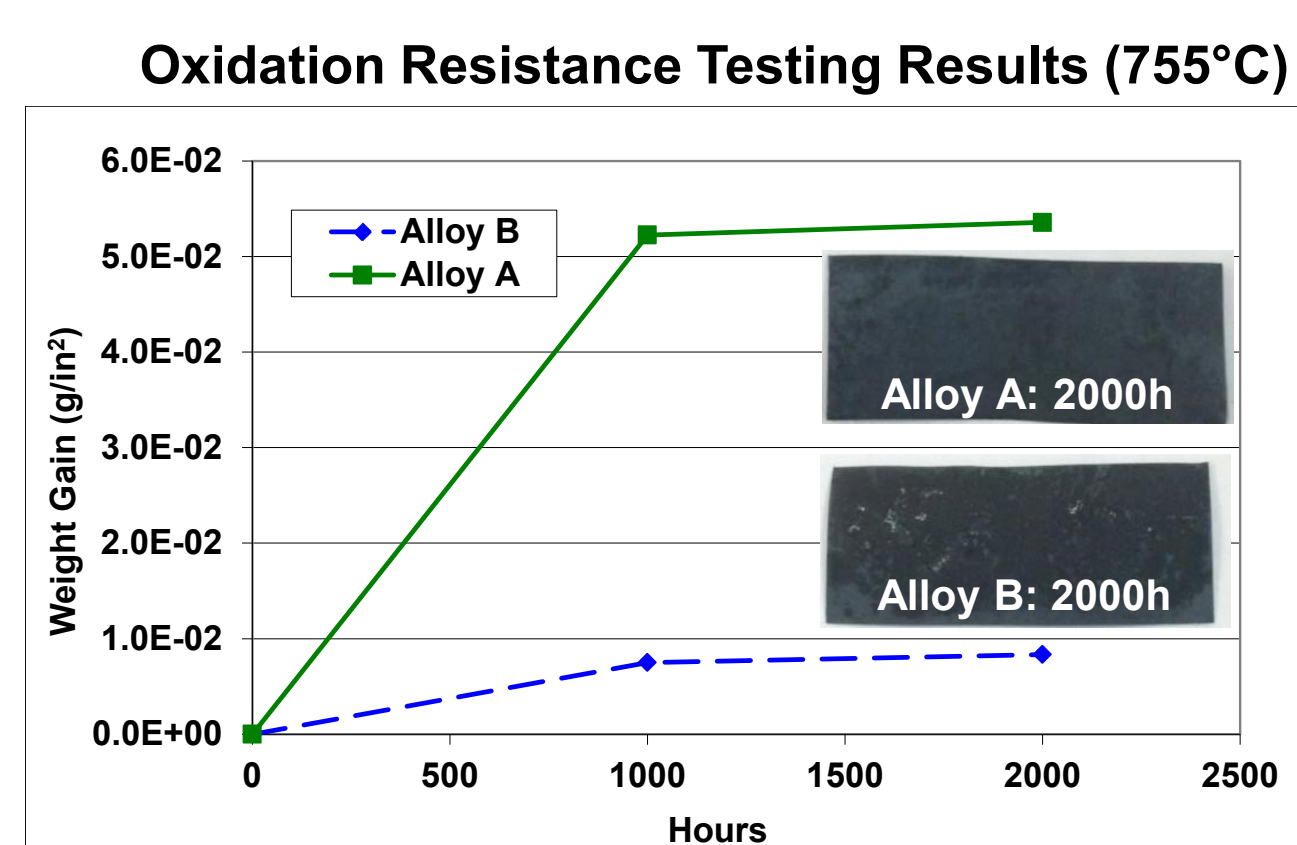


FCE's "10 kW" Subscale Test Facility

## Material of Construction Selection

### Key Material Selection Criteria:

- Oxidation Resistance
- Suitability for catalyst washcoating
- Joining via conventional methods
- Acceptable creep strength
- Availability
- Cost



Due to HX design features, maximum temperature is limited to ~770 °C. Therefore, high-Ni Super Alloys are not required.



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